

Gas-Liquid Flows and Phase Separation

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Strategic Research to Enable NASA's Exploration Missions

June 22 - 23, 2004
Cleveland, Ohio



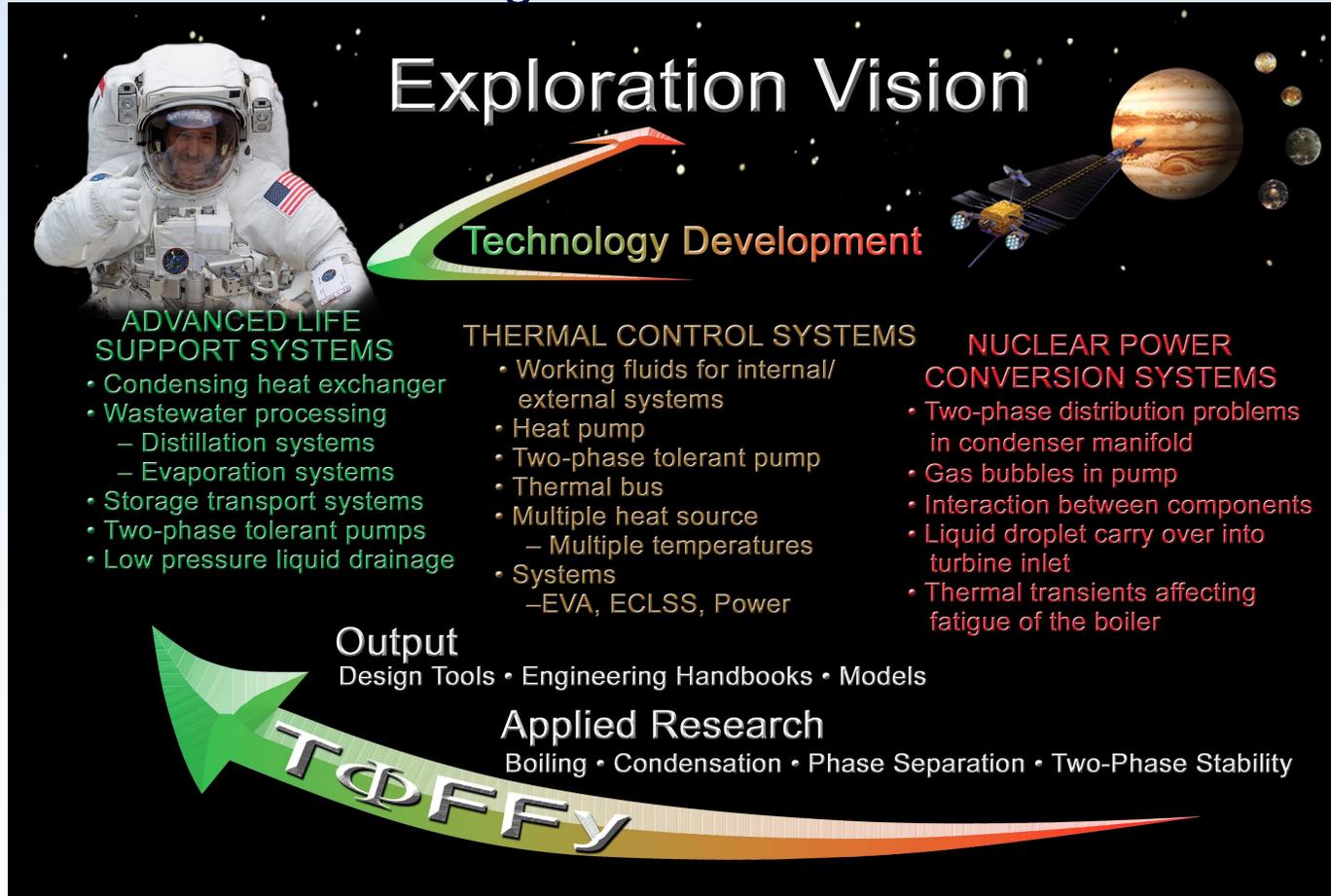
Common Issues for Space System Designers

- Ability to Verify Performance in Normal Gravity prior to Deployment.
- **System Stability***
- Phase Accumulation & Shedding
- **Phase Separation***
- Flow Distribution through Tees & Manifolds
- **Boiling Crisis***
- Heat Transfer Coefficient
- Pressure Drop

* Two Phase Flow Facility



Space-Based Technologies Using Two Phase Flow



Partial Listing of Where Gas-Liquid Flows are in Life Support Systems

Stream Type	Air Revitalization	Water Reclamation	Thermal Management	Solid Waste Management
Cabin Humidity Condensate	✓		✓	
Urine		✓		
Spills		✓		✓
Dish Washing		✓		
Laundry		✓		
Sabatier CO ₂ Reaction	✓			
Waste Solids Drying				✓
Food Processing		✓		✓

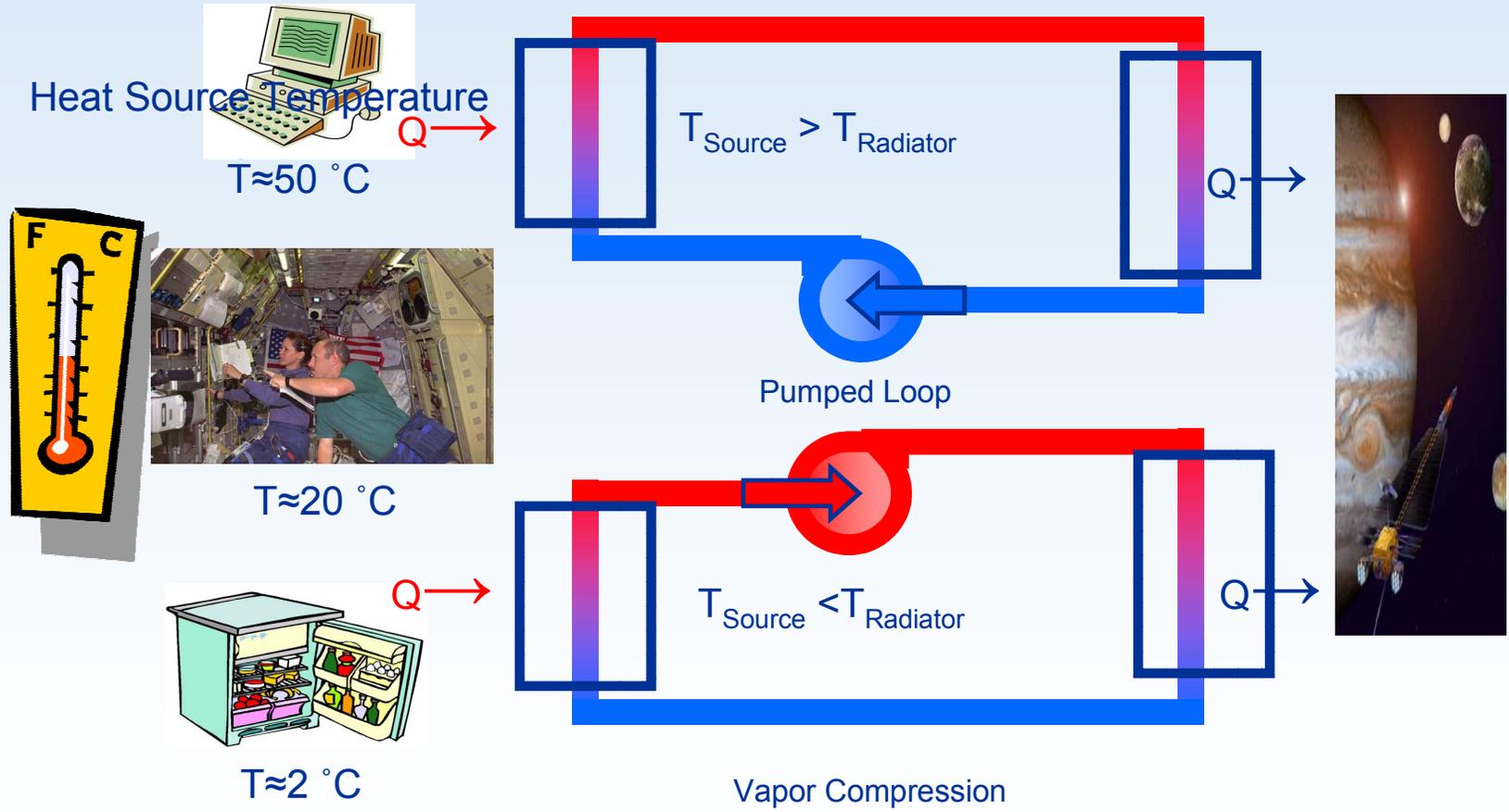


Life Support Systems

- Commonality of Source Stream
 - Aqueous-based Working Fluid (Water)
 - Into Waste Water Tank
 - Low Pressure Inlet
 - Gas Phase Present
 - Particulate Matter may be Present
- Differences
 - Dissolved Matter → Fluid Property Effects
 - Batch vs. Continuous Input
 - Flow Rates
 - Void Fraction

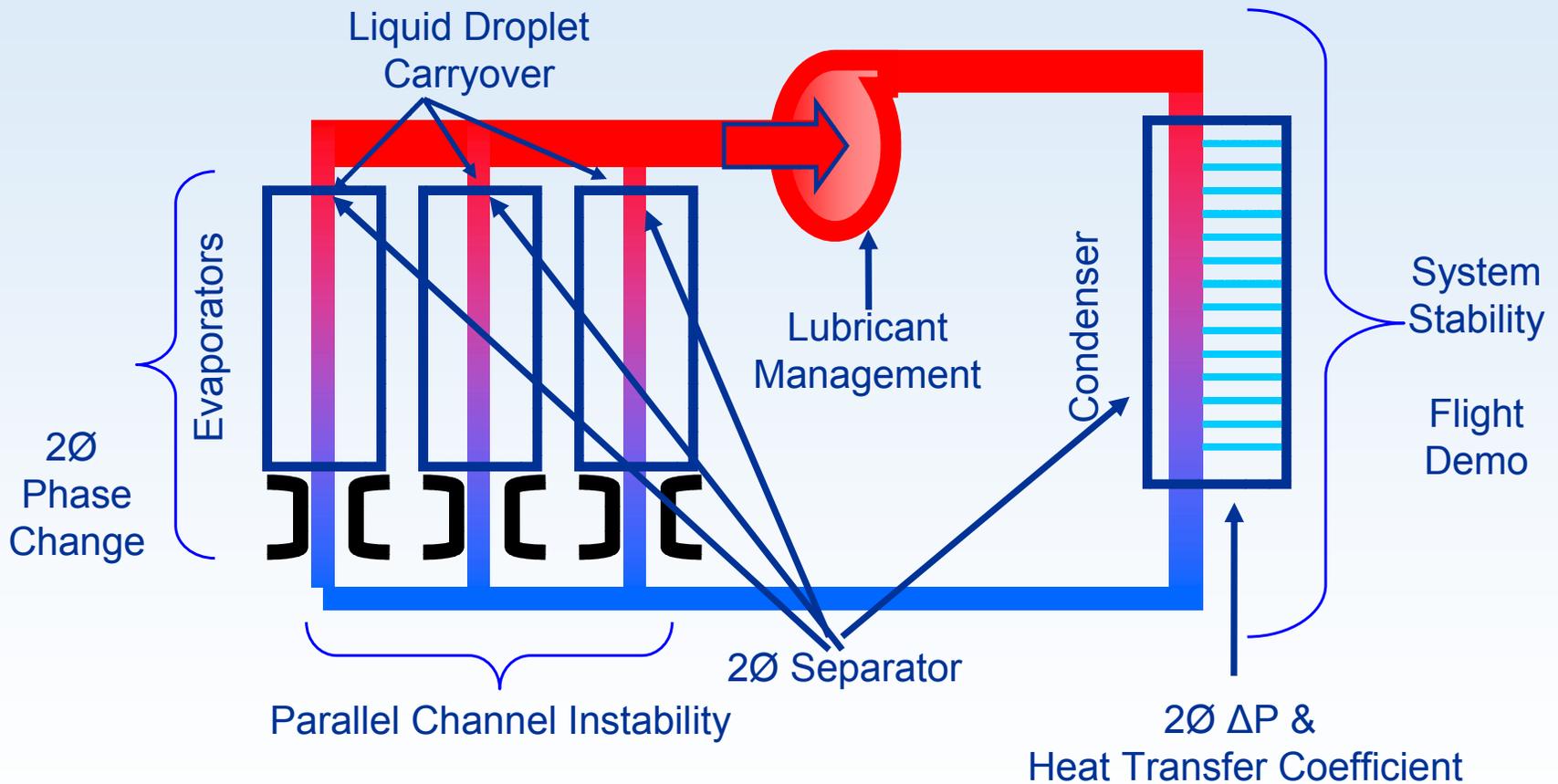


Thermal Management Systems



Vapor Compression Cycle

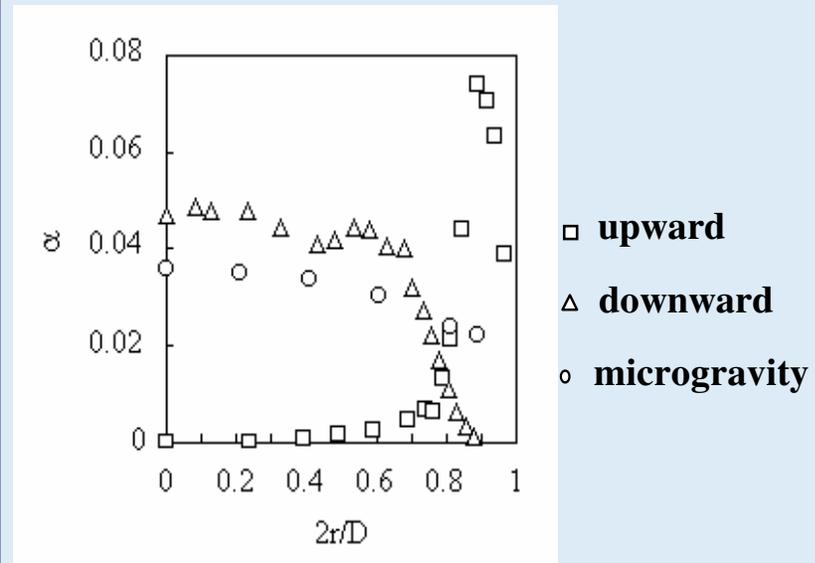
Two Phase Issues



The Effect of Reduced Gravity on Gas-Liquid Flows *Negating the Effect of Buoyancy*

- Axisymmetric flows
- Reduced Hydrostatic Pressure
- Spherical Bubbles vs. Ellipsoid
- No Gravity-Induced Shearing:
 - Gas Phase Rising relative to Liquid Falling
- Co-flow of Gas and Liquid Phases.

Radial void fraction distributions



What Do We Know? Flow Regimes

- 3 (½) Flow Regimes: Bubble, Slug, Annular (Transitional Slug Annular)
- Multiple Models that work well
 - Constant Void Fraction
 - Weber Number Model
 - Suratman Number Criteria

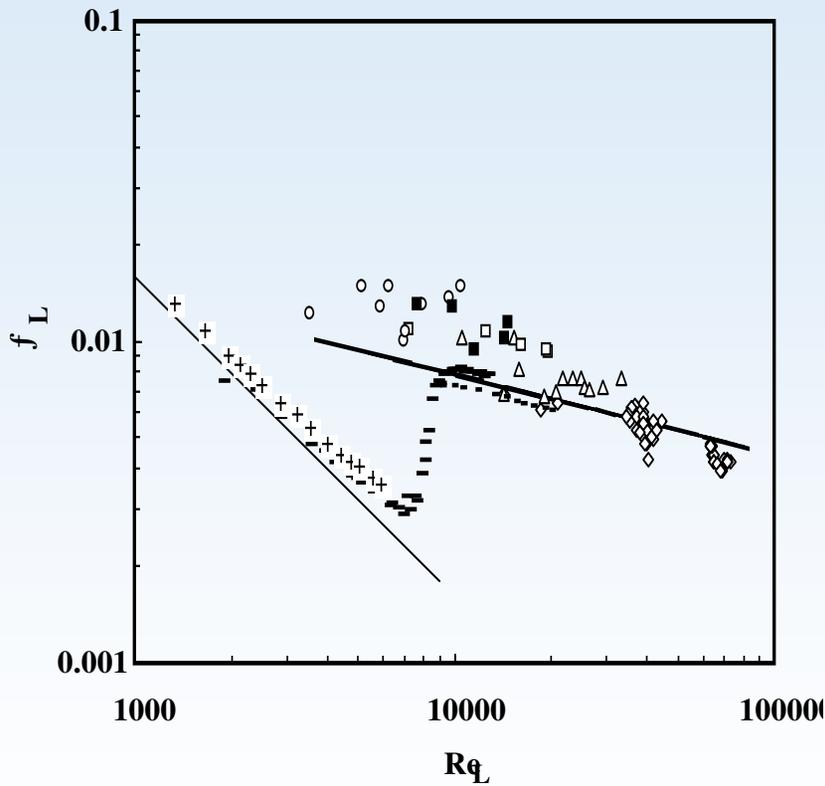


What Do We Know? Pressure Drop

- Modified Homogenous Equilibrium Model works well
 - Mixture Density
 - Mixture Velocity
 - Liquid Viscosity



Wall Friction Factors f_L in Bubbly Flow:



Reduced Gravity Two Phase Flow:

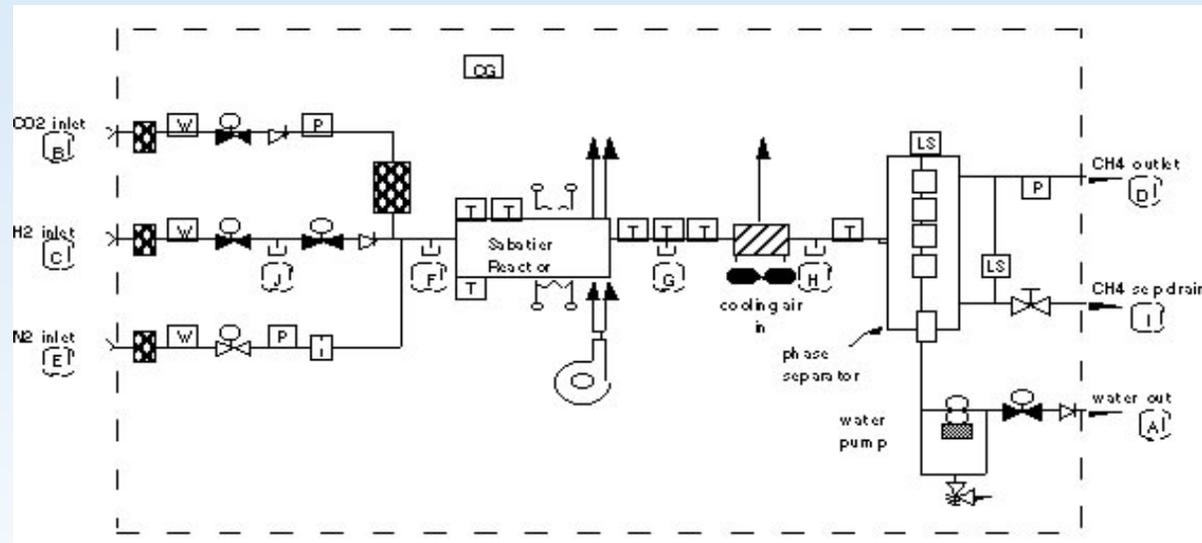
- $D=6$ mm, □ $D=10$ mm, △ $D=19$ mm,
- $D=12.7$ mm, ◇ $D=40$ mm

Single-Phase Flow:

- + $D=6$ mm, _ $D=10$ mm, - $D=19$ mm

— Blasius, — Poiseuille relationship

Example: Sabatier Reactor



2Ø Issues

- Separator
- Liquid in Gas Outlet Stream
 - Detection
 - Response
- Influence of Fines

Crew Exploration Vehicle Thermal Management System

- Capsule-type vehicle
- Functional during Orbital, Re-entry, and Post-Landing Phases
- Closed Loop System – Desire No Flash Evaporators
- Heat Load Estimate
 - Fuel Cells: 7 kW at 50 °C
 - Electronics: 3 kW at 40 °C
 - Cabin: 0.5 kW at 7 °C
- Limit Total Radiator Area < 200 ft²
- Body Mounted Radiator
- Working Fluid
 - Non-Toxic
 - Non-Corrosive
 - Low Freezing Point



Why Separate?

- **Critical Process or Component that is intolerant of one Phase**
 - Centrifugal pumps with gas bubbles
 - Phase Specific Sensors, i.e., hot wires
 - Biological media negatively impacted by gas
- **Better System Performance**
 - Condensers Work Better if no liquid present at inlet.
 - Control of Phase Distribution into a manifold



Requirements to Consider

- Available Power
 - Mars Transfer Vehicle has MW but for propulsion
 - CEV has up to 10 kW
- Vibration
 - Wear & tear
 - Noise
- System Life
 - Most will be Life of Mission or Vehicle
 - Some systems may have cleanliness/sterile concerns
- Separator Life
- Flow Rate range
 - ml/min to l/min



Requirements to Consider

- Acceleration Environments
 - Pre Launch 1 G
 - Launch – hi-G's
 - Transit - microgravity
 - De-Orbit – hi-G's
 - Moon (1/6 G) or Mars (3/8 G)
 - Post Landing 1 G
- Degree of Separation Desired
- Contamination Sensitivity
 - Separation process negatively impacted by solids or immiscible 2nd liquid phase
- Tolerance of “Slugging” or “flooding” Events
 - System capacitance
- Startup & Shutdown



Range of Separator Requirements

Stream Type	Near Continuous or Batch	Inlet Void Fraction
Cabin Humidity Condensate	Continuous	?
Urine	Batch	Low
Dish Washing	Batch	Low-Initially
Laundry	Batch	Low - Initially
Sabatier CO ₂ Reaction	Continuous	High
Waste Solids Drying	Continuous	High
Food Processing	Batch	High
Bioreactor	Continuous	Low



Mechanical Phase Separation

- Centrifuge – Very high G's
 - Spin outside housing
 - Spin internal float
- Use rotational acceleration to also develop “hydrostatic” pressure rise to pump liquid
 - Rotary Fluid Management Device (Sundstrand)
 - Two Phase Pump (Foster-Miller)
 - MOBI



Passive Separation: Membranes

- Use of Hydrophilic Membranes and Surfaces to position liquid interface and withdraw liquid.
- Liquid Acquisition Devices (LAD's) are used in upper stage propellant tanks to ensure start of rocket motor.
- Gas Phase Breakthrough based on bubble point or LaPlace Eqn using membrane pore size.
- Prone to contamination.



Passive Separation: Inertial

- Phase Separation achieved due to inertial differences in liquid and gas phase inertia

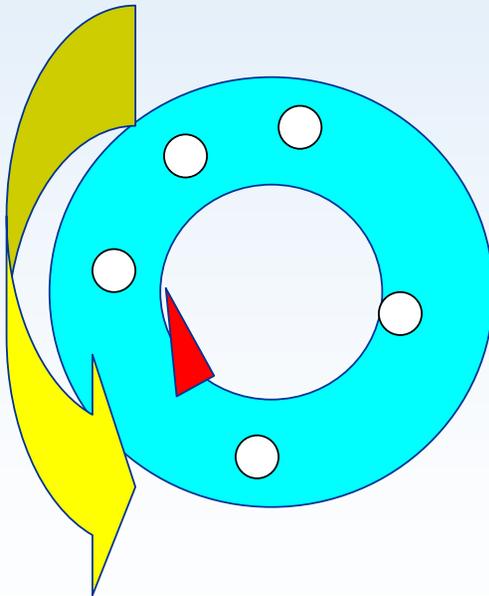
Bubble Flow through Tee

Gas Accumulation in
Vena Contracta



Passive Separation: Inertial

- Phase Separation achieved due to inertial differences in liquid and gas phase inertia



Passive Separation: Cyclonic

- Two Phase Flow Injected Tangentially into Cylinder.
- Separation driven by Flow
- Cyclones designed for microgravity will work well in multiple gravity levels



Summary

- Guidance similar to “A design that operates in a single phase is less complex than a design that has two-phase flow ”¹ is not always true considering the amount of effort spent on pressurizing, subcooling and phase separators to ensure single phase operation.
- While there is still much to learn about two-phase flow in reduced gravity, we have a good start.
- Focus now needs to be directed more towards system level problems.

¹ Graf, J., Finger, B., Daus, K., “**Life Support Systems for the Space Environment: Basic Tenets for Designers Rev. A,**” <http://advlifesupport.jsc.nasa.gov/documents/lsttenets.doc>, 2003.



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